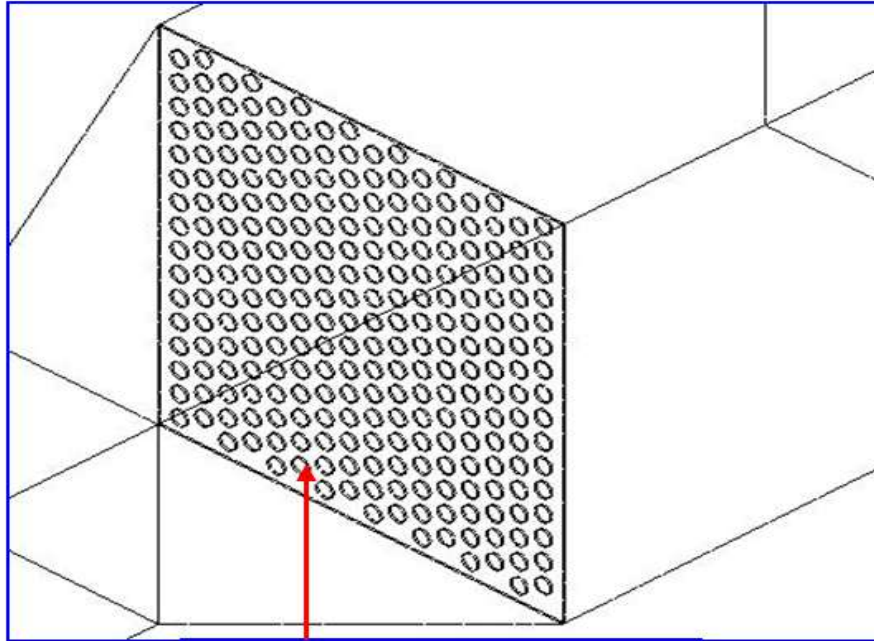
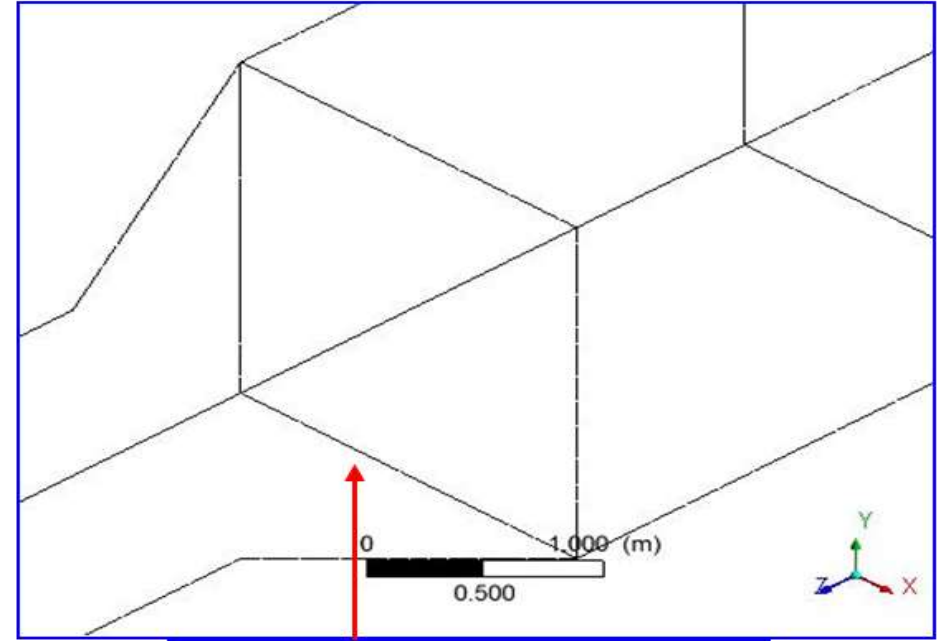


# DETAIL OF RAMAGUNDAM ST-II ESP: GD Screen modeling

SAME SIZE DOMAIN



DOMAIN WITH 10 MM GD  
SCREEN WITH  
STAGGERED HOLE  
ARRANGEMENT



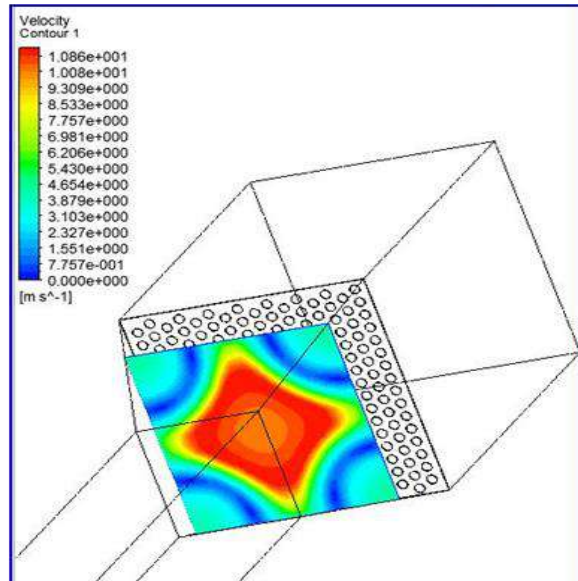
DOMAIN WITH POROUS JUMP  
APPROXIMATION OF  
UNIFORM HOLE  
ARRANGEMENT

Comparison of flow pattern between actual GD screen and porous jump plane-Geometry

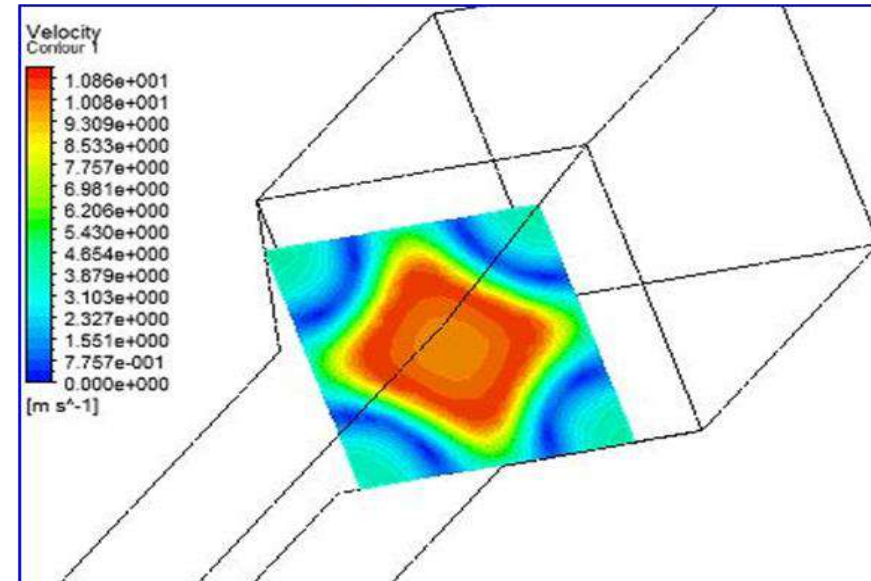
# DETAIL OF RAMAGUNDAM ST-II ESP: GD Screen modeling

## VELOCITY CONTOUR

### SECTION UPSTREAM OF GD SCREEN



DOMAIN WITH 10 MM GD  
SCREEN WITH  
STAGGERED HOLE  
ARRANGEMENT



DOMAIN WITH POROUS JUMP  
APPROXIMATION OF  
UNIFORM HOLE  
ARRANGEMENT

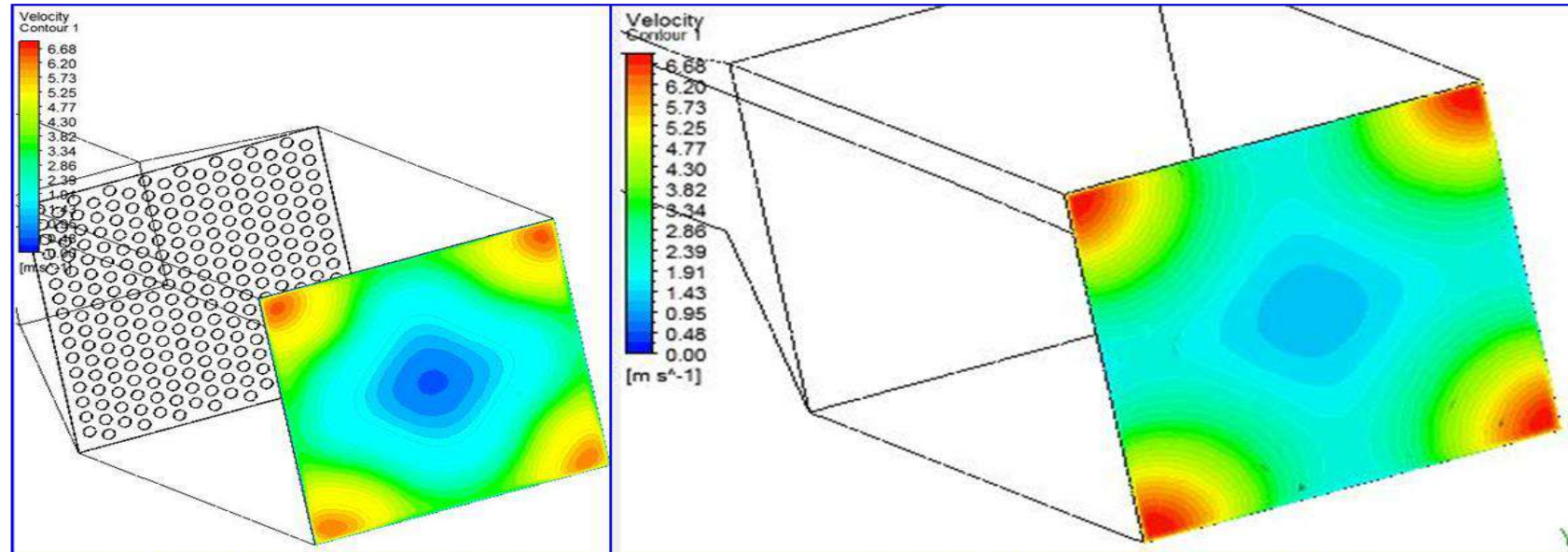
SIMILAR VELOCITY PROFILE IS OBSERVED IN BOTH THE CASES

Comparison of flow pattern between actual GD screen and porous jump plane-Result

# DETAIL OF RAMAGUNDAM ST-II ESP: GD Screen modeling

## VELOCITY CONTOUR

### SECTION DOWNSTREAM OF GD SCREEN (OUTLET)



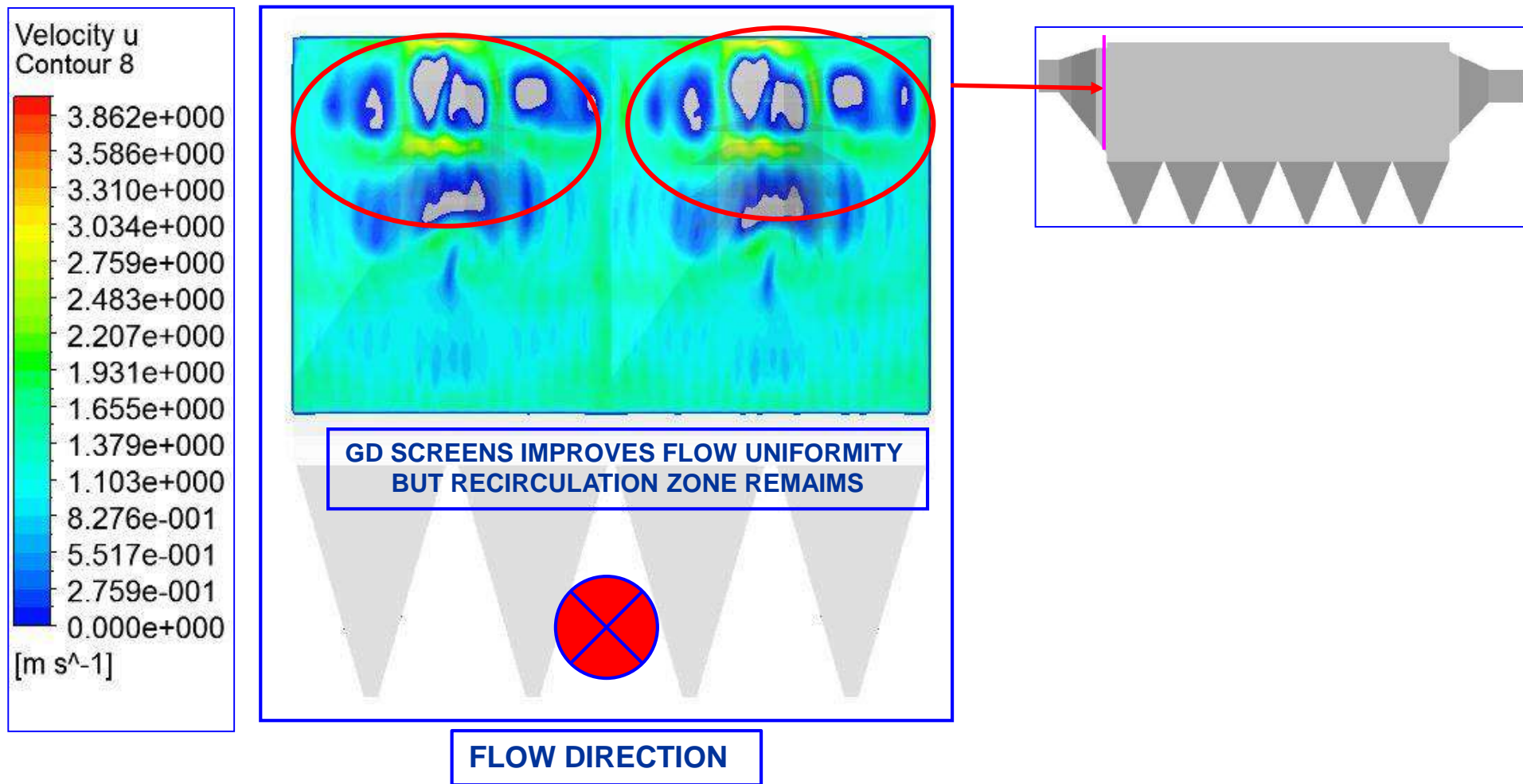
DOMAIN WITH 10 MM GD  
SCREEN WITH  
STAGGERED HOLE  
ARRANGEMENT

DOMAIN WITH POROUS JUMP  
APPROXIMATION OF  
UNIFORM HOLE  
ARRANGEMENT

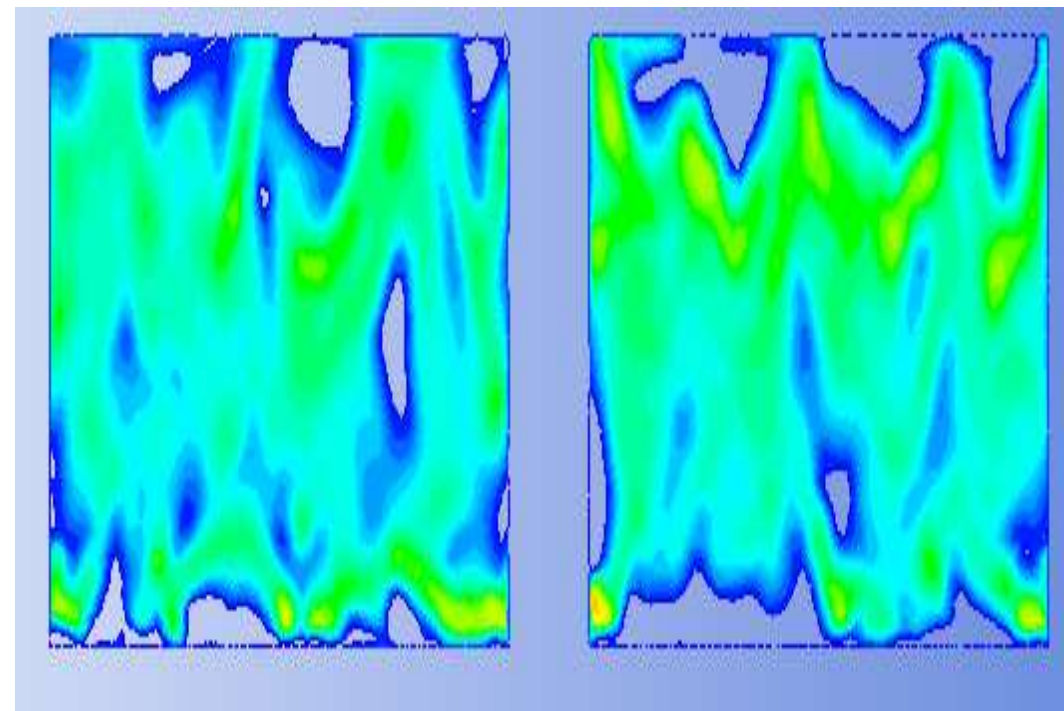
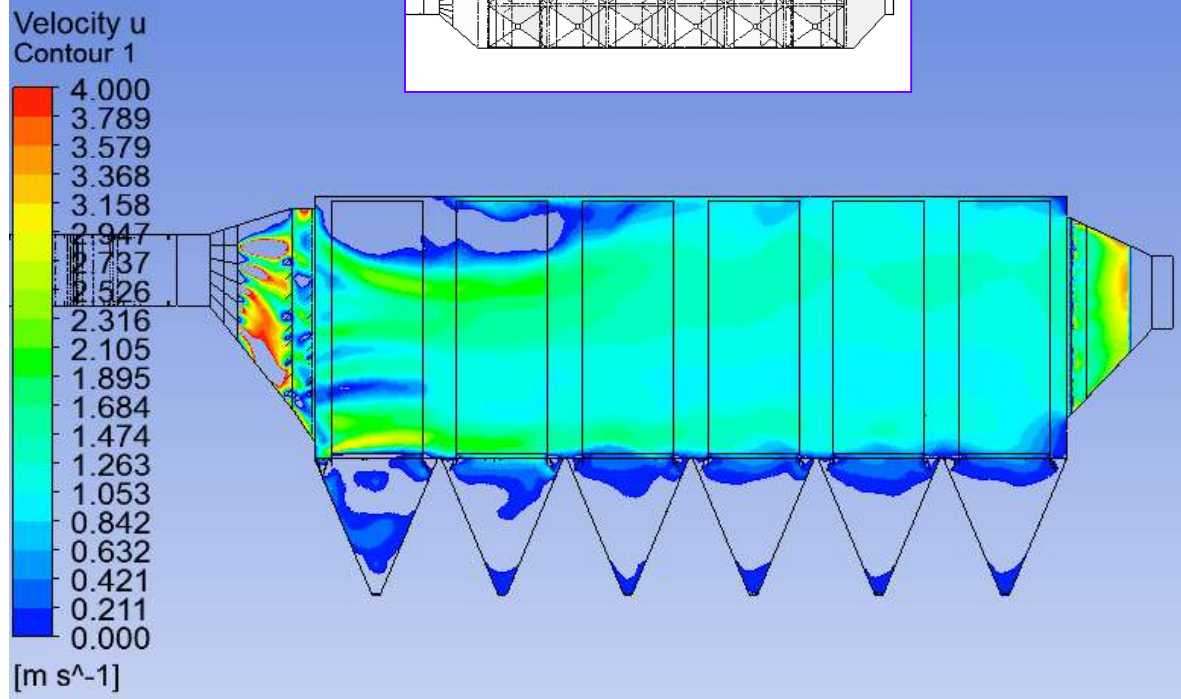
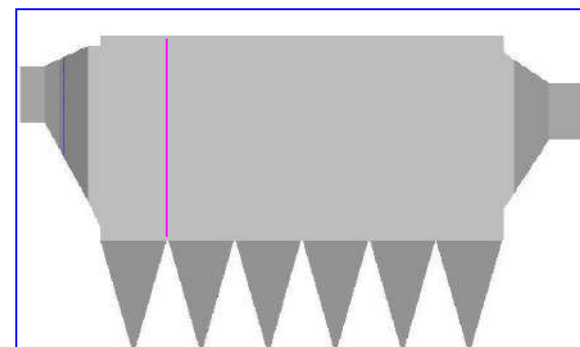
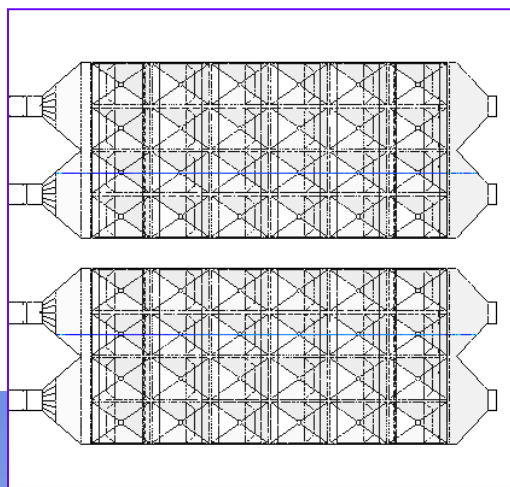
SIMILAR VELOCITY PROFILE IS OBSERVED IN BOTH THE CASES

**Conclusion: Porous jump can be used in place of actual simulation of GD screen**

## Flow separation after GD Screen

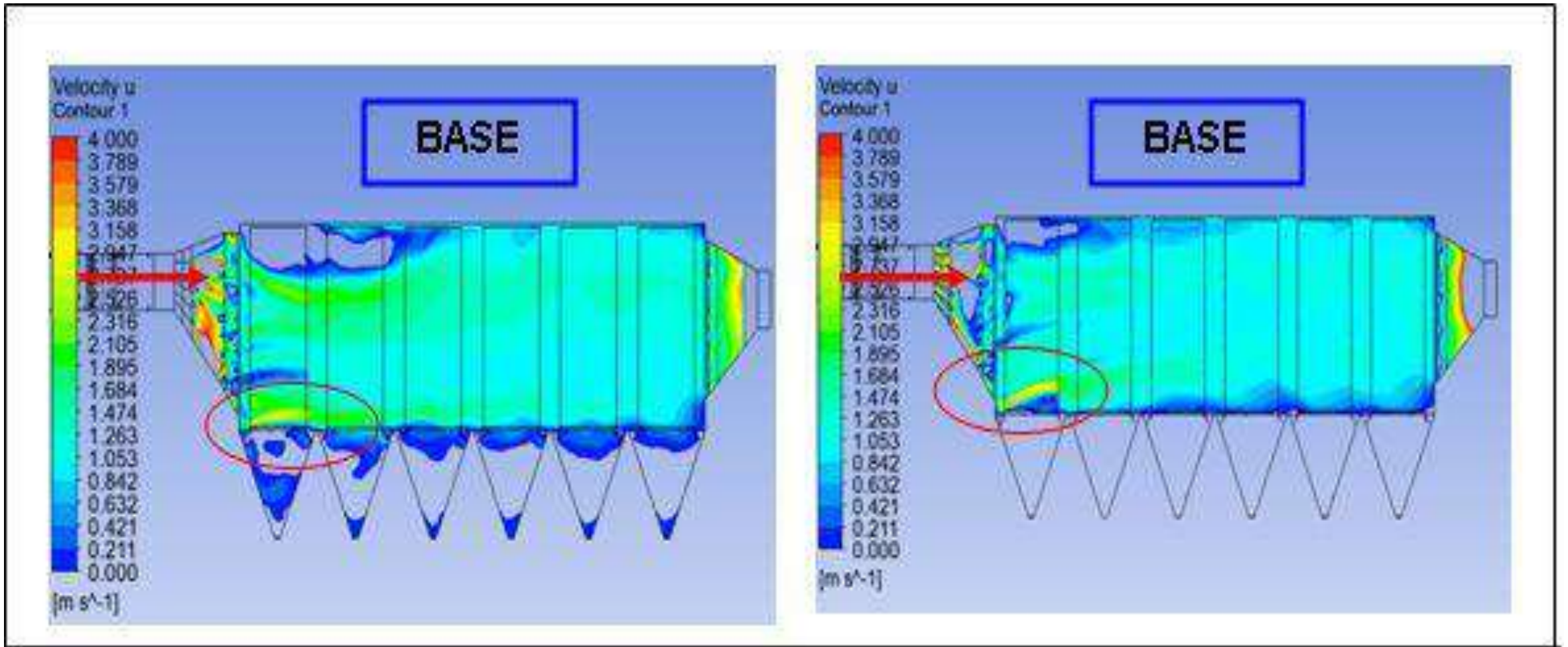


# DETAIL OF RAMAGUNDAM ST-II ESP: Results- Flow in 1<sup>st</sup>/2<sup>nd</sup> fields



# DETAIL OF RAMAGUNDAM ST-II ESP: Results-Flow in 1<sup>st</sup> /2<sup>nd</sup> Field

## Recirculation zones and high velocity over first field hoppers



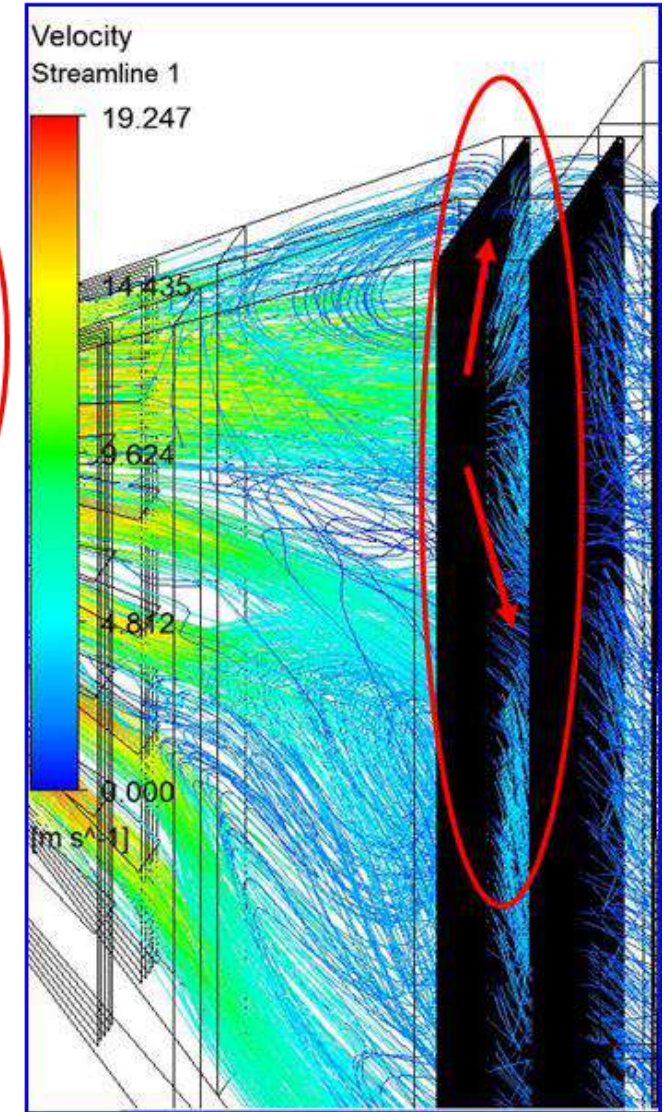
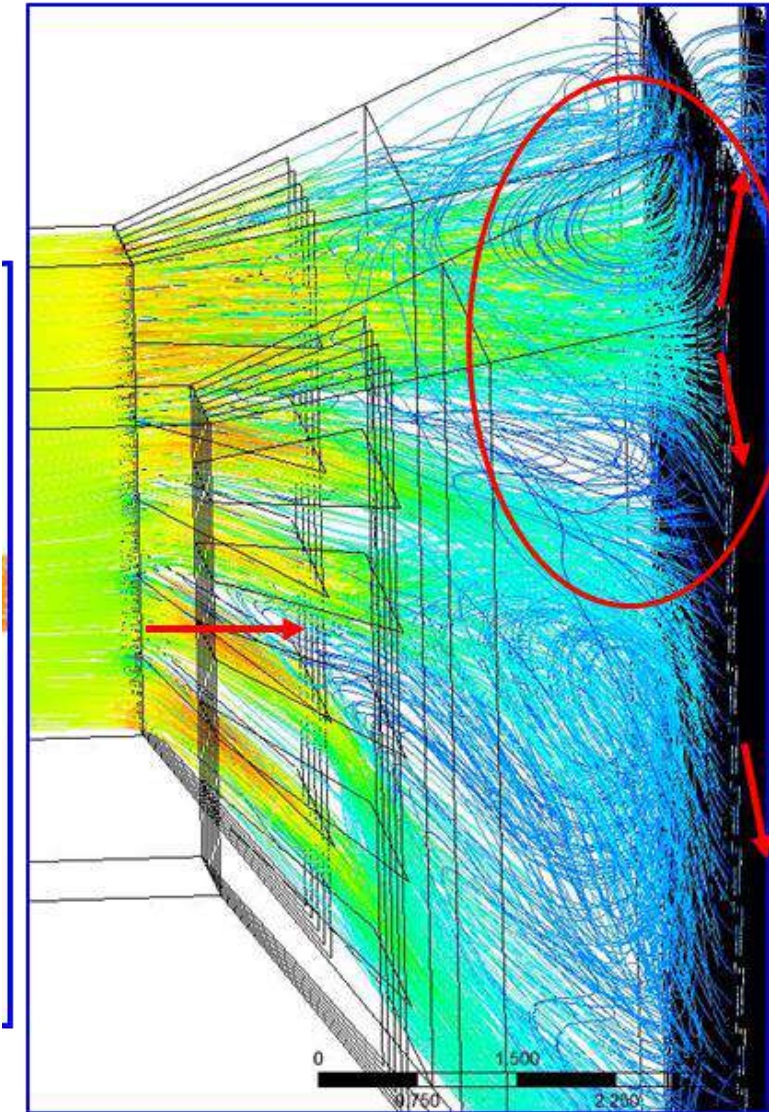
### Summary of flow pattern inside ESP

- Presence of stagnation zone after splitter/diffuser plate
- Presence of stagnation zone in first two fields
- 38 % of cross-sectional having more than 1.4\* Avg. velocity (ICAC Limit-1%)
- Higher velocity above hopper

### Consequences:

- Low effective SCA
- Low precipitation efficiency
- High re-entrainment

# DETAIL OF RAMAGUNDAM ST-II ESP: Results: Flow around GD screens





## High Localized velocity

| Flue gas velocity pattern at cross-section after the first field |                             |                              |                            |
|--|-----------------------------|------------------------------|----------------------------|
| SN   | Average velocity, $V_{avg}$ | % Area $\leq 1.15 * V_{avg}$ | % Area $\leq 1.40 V_{avg}$ |
| 1  | 1.07                        | 43.53                        | 62.27                      |

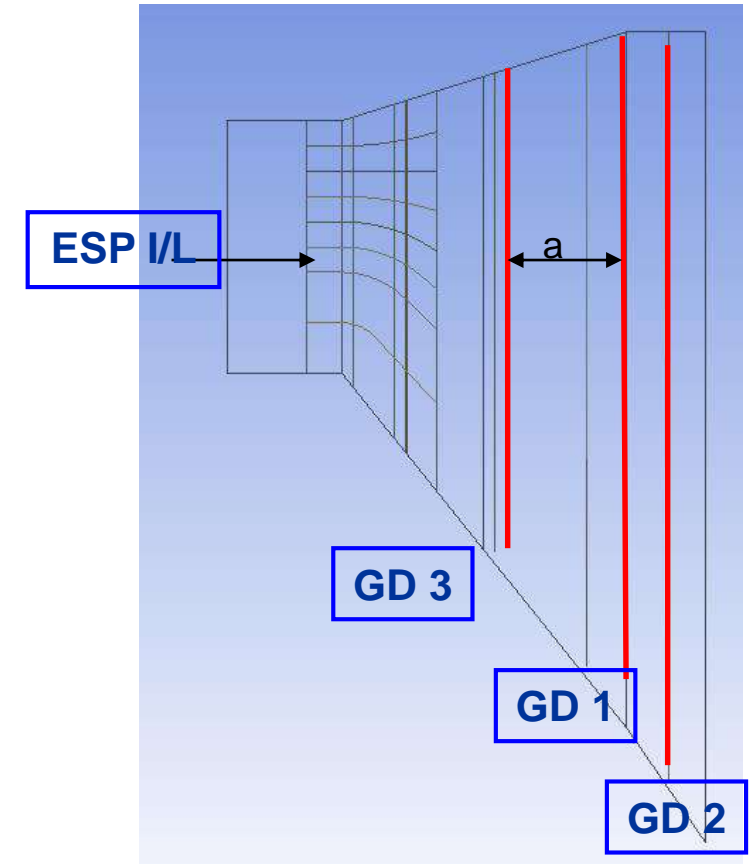
# **MODIFICATIONS STRATEGY FOR CORRECTING FLOW ABNORMALITY**



- To prevent flow separation after the splitter/diffuser plates
  - Modified designed splitter plate to reduce erosion and flow separation
  - At what distance (x) from plates flow separate, how it can be prevented
  - A GD screen ?? But it will add pressure drop in the system
- To prevent flow separation after GD screen:
  - Different amount of flow arrives at different part of GD screen
  - Blocking plates in GD screen causing stagnation zones in 1<sup>st</sup> and 2<sup>nd</sup> field
  - Can flow be made uniform without blocking screen, Multi hole GD screen
- To prevent re-entrainment from hopper
  - Existing hopper plates not able to prevent re-entrainment from hopper
  - New designed hopper plate

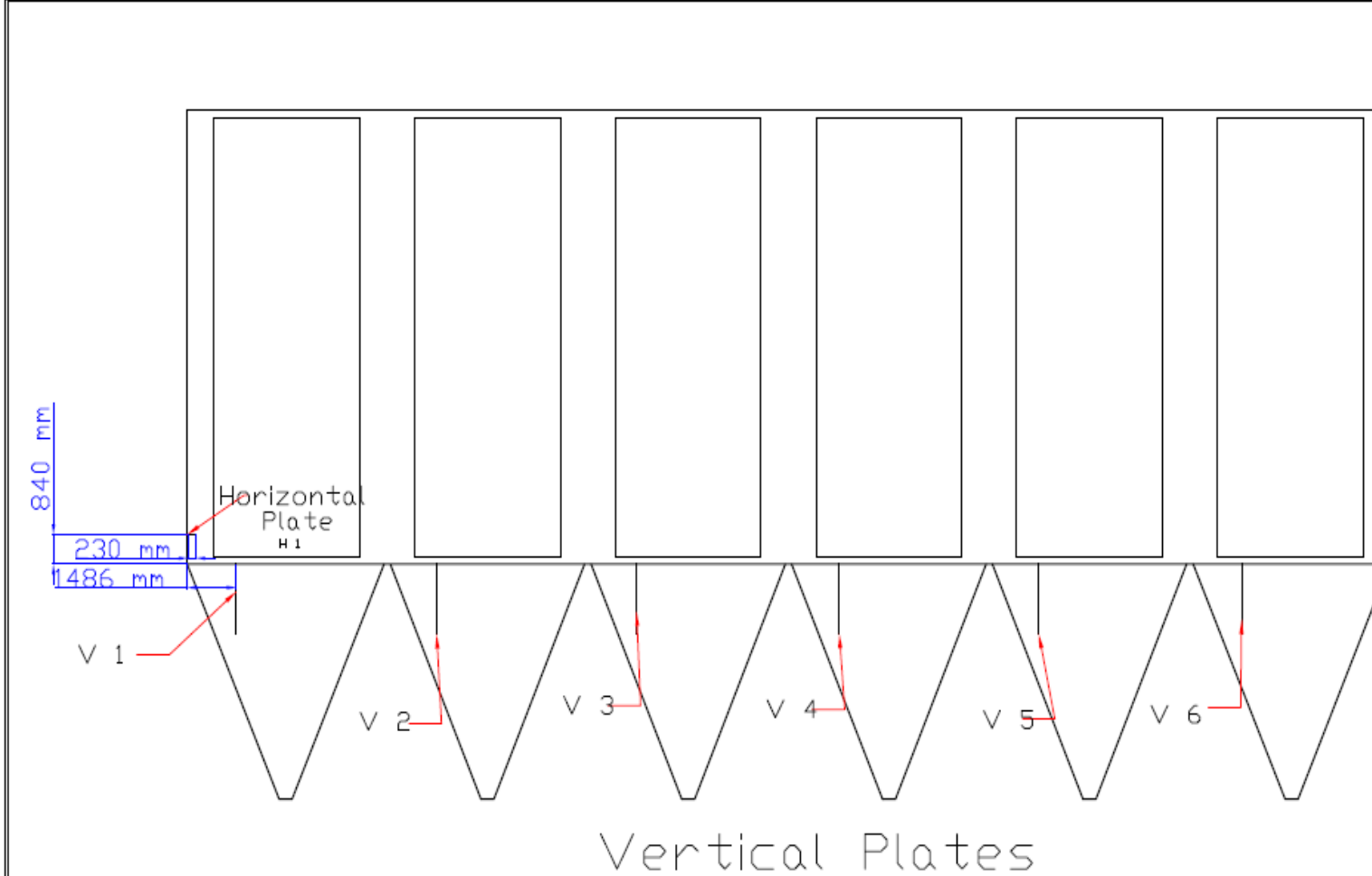
## Modification proposed

- Modified Splitter Plate design-similar to
- Addition of 3<sup>rd</sup> GD screen after splitter plate
- Graded porosity in existing GD Screens
- Hopper plates at appropriate location
- Replacement of all worn-out internals
- Flow reduction, Temperature reduction



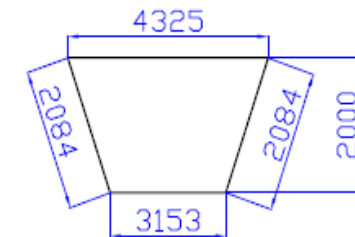
a- 1500 mm

# FINAL MODIFICATIONS

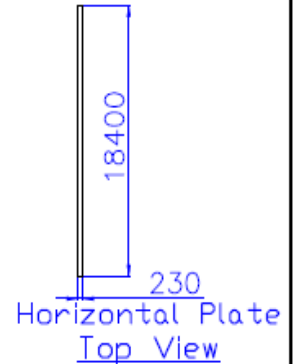


Remark:

1. 01 size of vertical plate in each hopper.
2. Thickness of sheet is 6 mm
3. All dimensions are in mm.



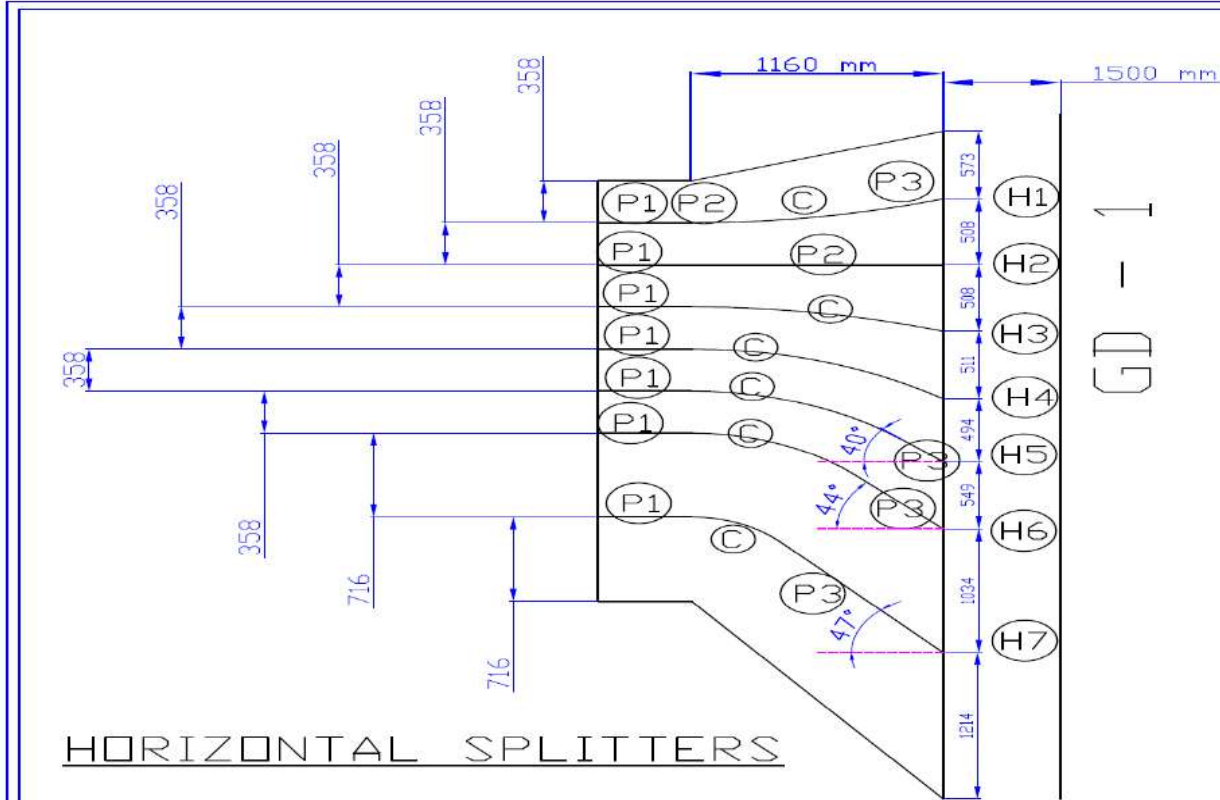
Vertical Plate



Horizontal Plate  
Top View

|                      |            |            |  |                     |           |
|----------------------|------------|------------|--|---------------------|-----------|
|                      | Name       | Date       | NTPC Energy Technology Research Alliance |                     |           |
| DRAWN BY             | A Sutrakar | 11.10.2017 | Title                                    |                     |           |
| CHECKED BY           | A Sutrakar | 11.10.2017 | Hopper Plates                            |                     |           |
| APPROVED BY          | S Karnakar | 11.10.2017 | Size                                     | Drawing Title       | SHEET Rev |
| NOT TO SCALE DRAWING |            |            | Ao                                       | Netra/CFD/RG/ESP/03 | 1 OF 1 02 |

# FINAL MODIFICATIONS



| Horizontal Splitter |            |        |           |                       |           |
|---------------------|------------|--------|-----------|-----------------------|-----------|
| SL. NO              | Horizontal | Radius | Cord Leng | Arc Length/Length     | Thickness |
| 1                   | H1         | P1     | -         | As per site condition | 6         |
|                     |            | P2     | -         | -                     | -         |
|                     |            | C      | 4532      | 1366                  | 1542      |
|                     |            | P3     | -         | -                     | -         |
| 2                   | H2         | P1     | -         | As per site condition | 6         |
|                     |            | P2     | -         | 1533                  | 6         |
|                     |            | C      | -         | -                     | -         |
|                     |            | P3     | -         | -                     | -         |
| 3                   | H3         | P1     | -         | As per site condition | 6         |
|                     |            | P2     | -         | -                     | 6         |
|                     |            | C      | 4532      | 1366                  | 1542      |
|                     |            | P3     | -         | -                     | -         |
| 4                   | H4         | P1     | -         | As per site condition | 6         |
|                     |            | P2     | -         | -                     | -         |
|                     |            | C      | 2367      | 1410                  | 1573      |
|                     |            | P3     | -         | -                     | -         |
| 5                   | H5         | P1     | -         | As per site condition | 6         |
|                     |            | P2     | -         | -                     | -         |
|                     |            | C      | 1749      | 1207                  | 1575      |
|                     |            | P3     | -         | -                     | 43        |
| 6                   | H6         | P1     | -         | As per site condition | 6         |
|                     |            | P2     | -         | -                     | -         |
|                     |            | C      | 1260      | 948                   | 1234      |
|                     |            | P3     | -         | -                     | 462       |
| 7                   | H7         | P1     | -         | As per site condition | 6         |
|                     |            | P2     | -         | -                     | -         |
|                     |            | C      | 643       | 514                   | 668       |
|                     |            | P3     | -         | -                     | 1175      |

Note: All dimensions are in mm

Legends:

- V Vertical
- C Curved Baffles
- P Straight Plate

Remarks:

C1 to C5 is in increasing order of size.

Note: All dimensions are in mm

Legends:

- V : Vertical
- C : Curved Baffles
- P : Straight Plate

C1 to C5 is in increasing order of size.

Note:- The length of Straight plate P1 is to be taken as per the space available between end of the expansion joint and starting point of the funnel

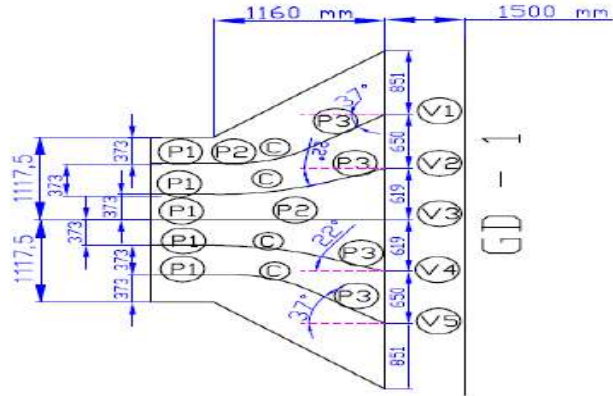
Remarks:  
All dimensions are in mm.

LEGENDS:

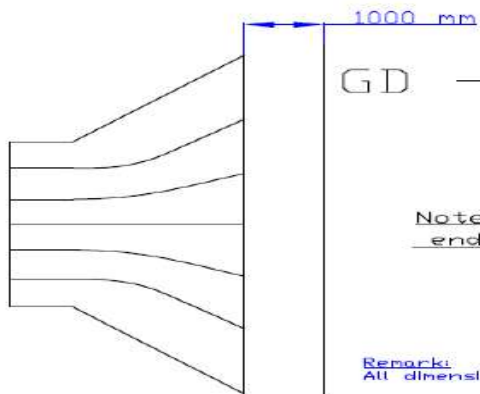
- Dimension Line
- Reference Line

|                      |                      |            |   |
|----------------------|----------------------|------------|---|
| DRAWN BY             | Name                 | Date       | NTPC Energy Technology<br>Research Alliance |
| CHECKED BY           | A.K. Sutrakar        | 11.10.2017 |   |
| APPROVED BY          | S. Karmakar          | 11.10.2017 |   |
| NOT TO SCALE DRAWING |                      |            | Title<br>Horizontal Splitters               |
| Size                 | Drawing Title        | SHEET      | Rev   |
| Ao                   | Netra/CFD/RO/ESP/01d | 1 OF 1     | 02  |

# FINAL MODIFICATIONS



VERTICAL SPLITTERS



| Vertical Splitter |          |        |             |                   |                       |   |
|-------------------|----------|--------|-------------|-------------------|-----------------------|---|
| SL. NO            | Vertical | Radius | Cord Length | Arc Length/Length | Thickness             |   |
| 1                 | V1       | P1     | -           | -                 | As per site condition | 6 |
|                   |          | P2     | -           | -                 | 162                   | 6 |
|                   |          | C      | 964         | 612               | 649                   | 6 |
|                   |          | P3     | -           | -                 | 548                   | 6 |
| 2                 | V2       | P1     | -           | -                 | As per site condition | 6 |
|                   |          | P2     | -           | -                 | -                     | - |
|                   |          | C      | 2427        | 937               | 986                   | 6 |
|                   |          | P3     | -           | -                 | 270                   | 6 |
| 3                 | V3       | P1     | -           | -                 | As per site condition | 6 |
|                   |          | P2     | -           | -                 | 1224                  | 6 |
|                   |          | C      | -           | -                 | -                     | - |
|                   |          | P3     | -           | -                 | -                     | - |
| 4                 | V4       | P1     | -           | -                 | As per site condition | 6 |
|                   |          | P2     | -           | -                 | -                     | - |
|                   |          | C      | 2427        | 937               | 958                   | 6 |
|                   |          | P3     | -           | -                 | 297                   | 6 |
| 5                 | V5       | P1     | -           | -                 | As per site condition | 6 |
|                   |          | P2     | -           | -                 | 162                   | 6 |
|                   |          | C      | 964         | 612               | 649                   | 6 |
|                   |          | P3     | -           | -                 | 548                   | 6 |

Note: All dimensions are in mm

Legends:

- V Vertical
- C Curved Baffles
- P Straight Plate

Remarks:

C1 to C5 is in increasing order of size.

Note: All dimensions are in mm

Legends:

- V : Vertical
- C : Curved Baffles
- P : Straight Plate
- C1 to C5 is in increasing order of size.

Note:- The length of Straight plate P1 is to be taken as per the space available between end of the expansion joint and starting point of the funnel

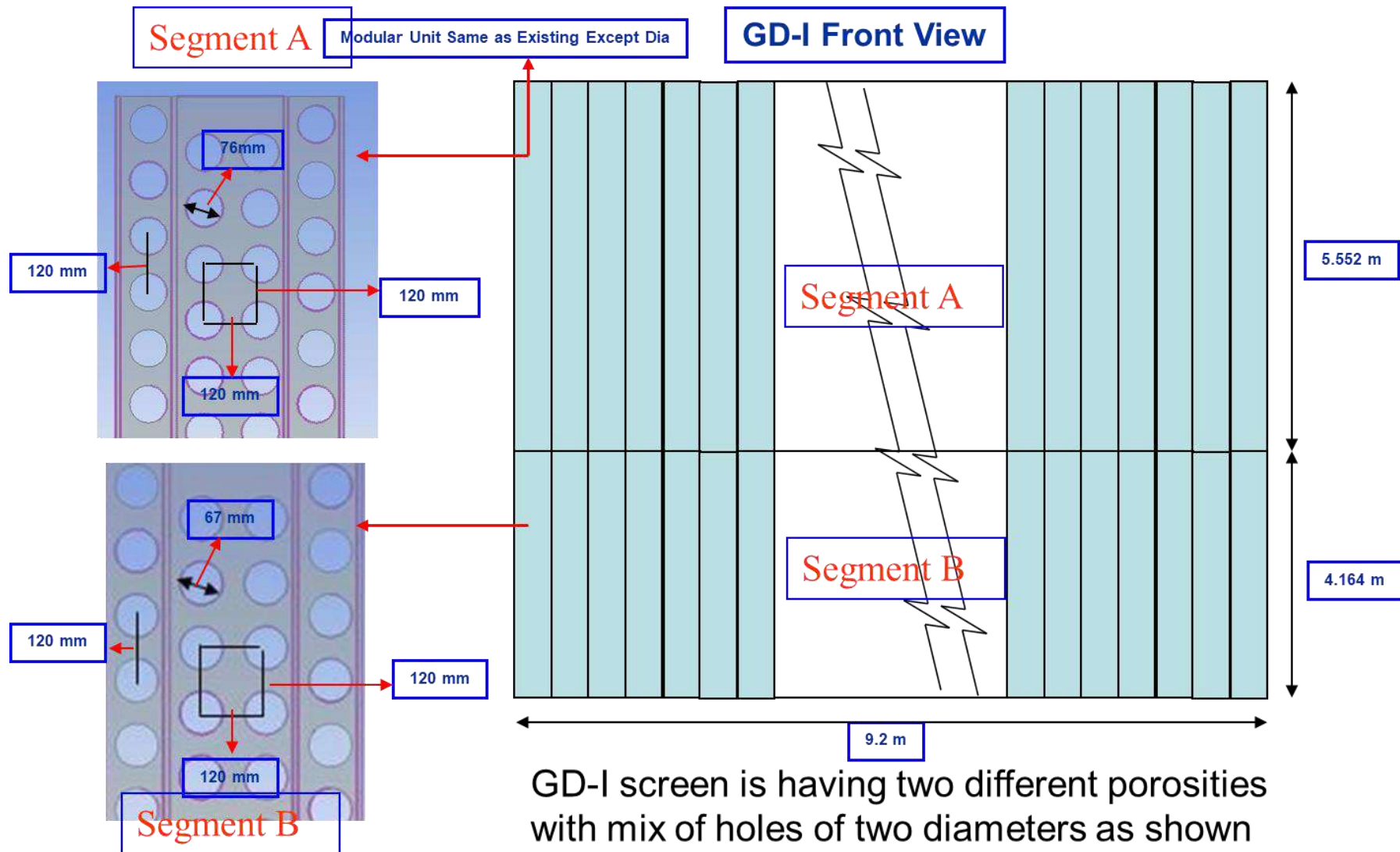
Remarks:  
All dimensions are in mm.

LEGENDS:

- Dimension Line
- Reference Line

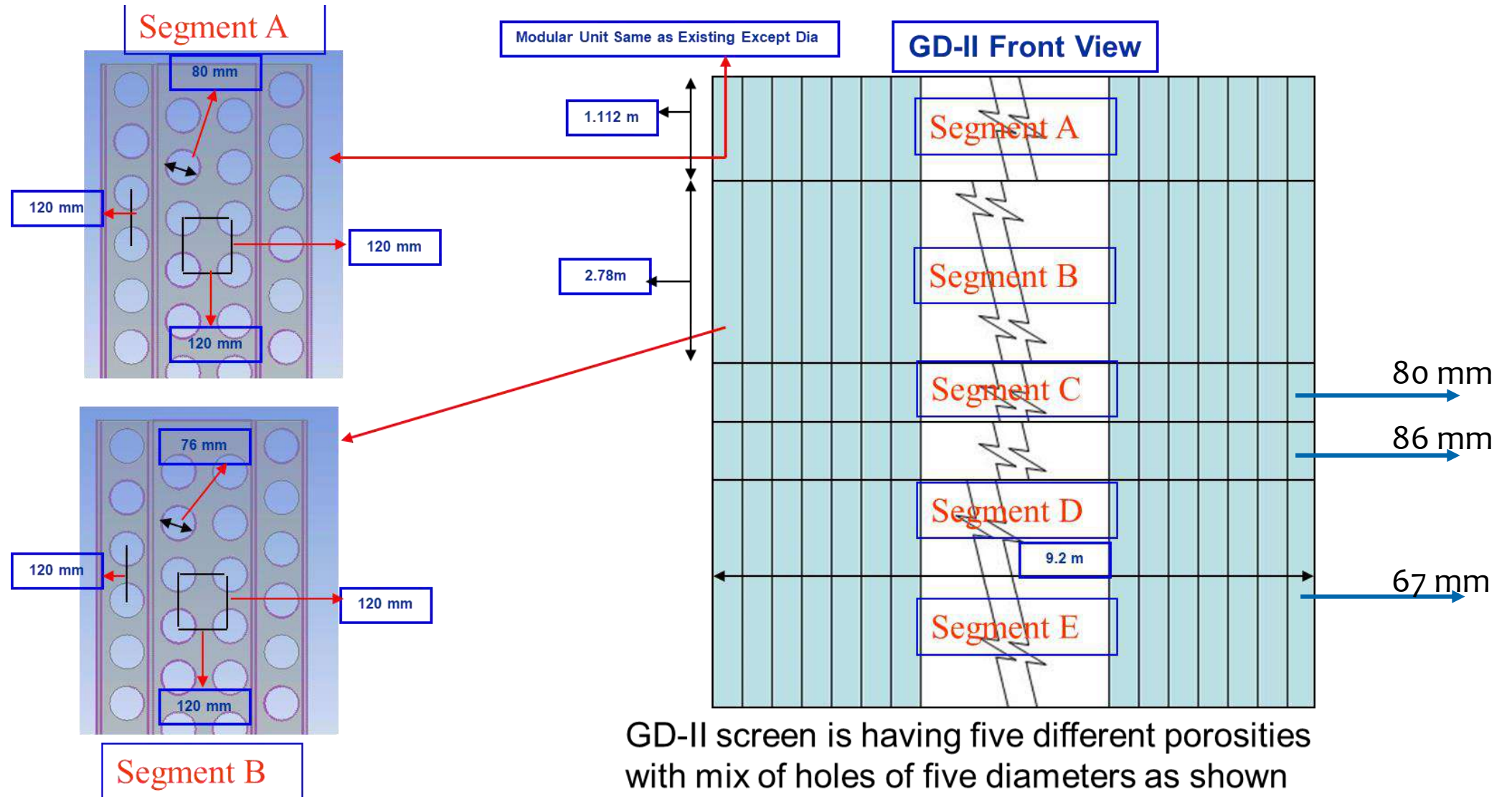
|                      |               |           |  |                      |           |
|----------------------|---------------|-----------|--|----------------------|-----------|
| DRAWN BY             | Name          | Date      | NTPC Energy Technology Research Alliance |                      |           |
| CHECKED BY           | A.K.Sutradhar | 1.10.2017 | Title Vertical Splitters                 |                      |           |
| APPROVED BY          | S.Karmakar    | 1.10.2017 | Size                                     | Drawing Title        | SHEET Rev |
| NOT TO SCALE DRAWING |               |           | Ao                                       | Netra/CFD/RG/ESP/01c | 1 OF 1 02 |

# FINAL MODIFICATIONS: Graded porosity GD Screen 1





# FINAL MODIFICATIONS: Graded porosity GD Screen 1

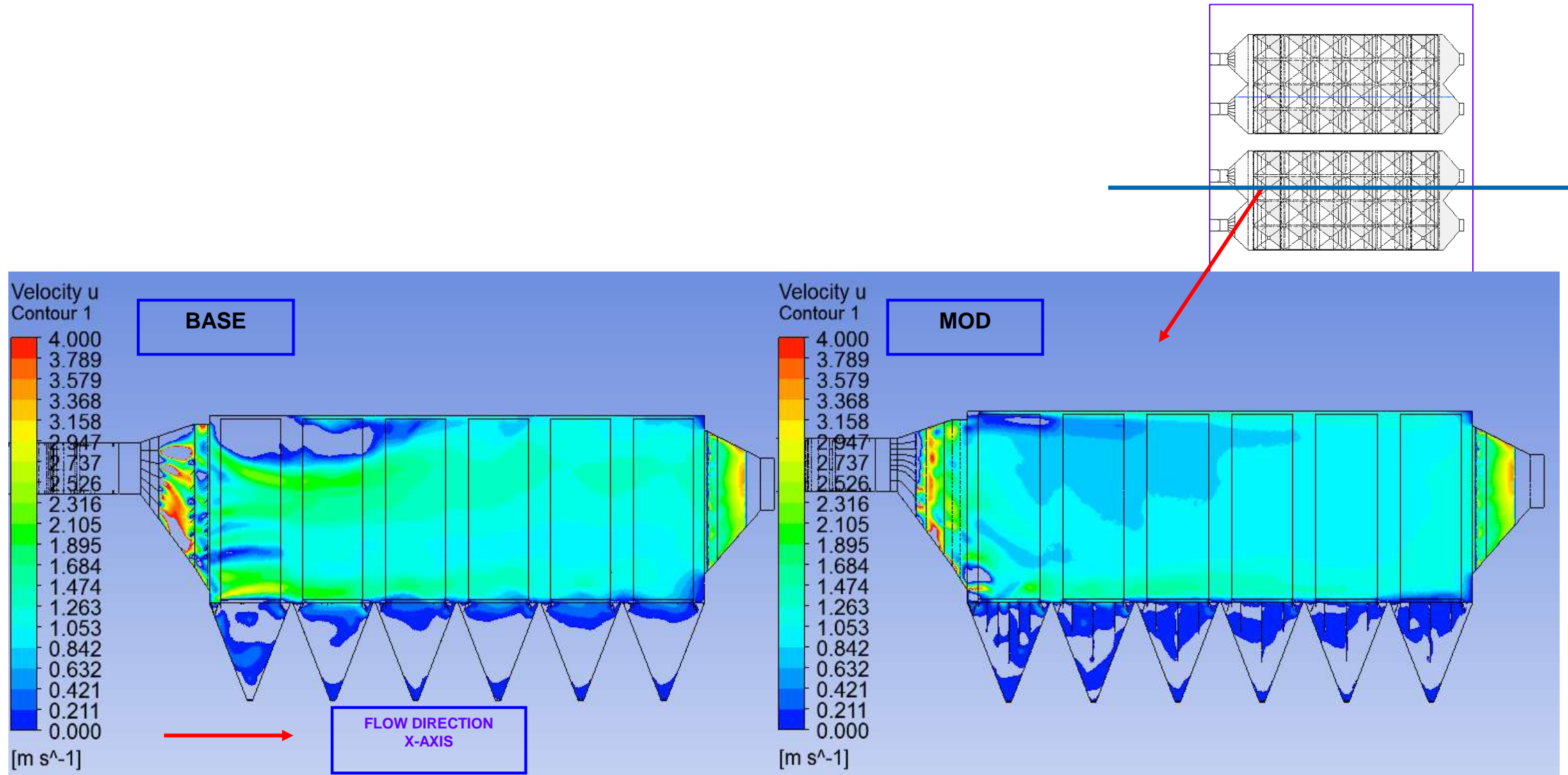


# **EFFECT OF MODIFICATION ON FLOW & ESTIMATED MODIFIED EFFICIENCY**





# EFFECT OF MODIFICATIONS ON FLOW PATTERN

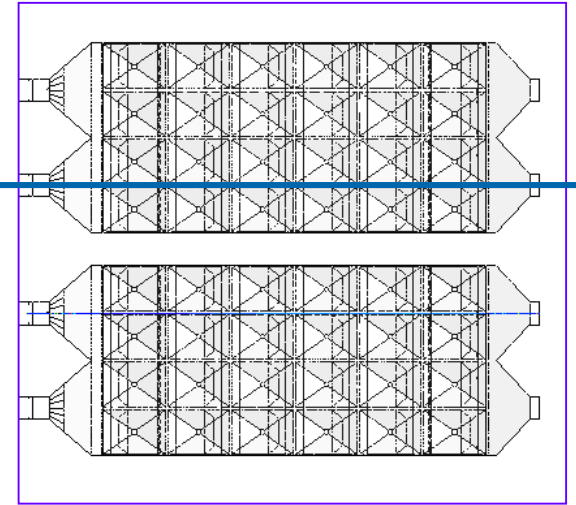
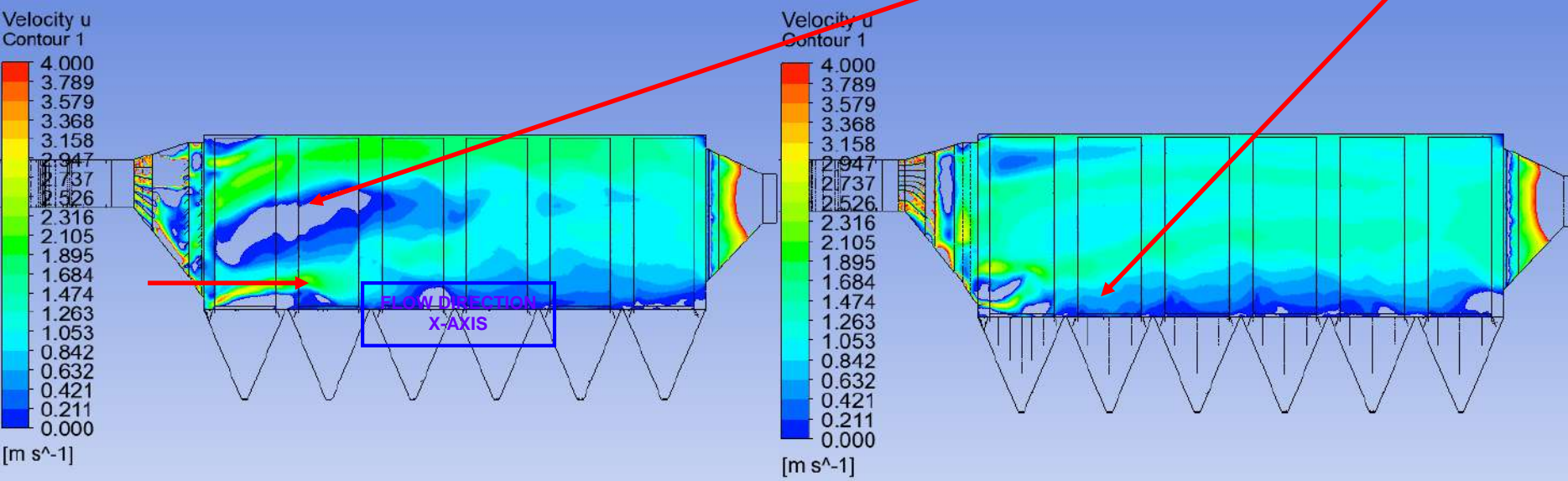


# EFFECT OF MODIFICATIONS ON FLOW PATTERN

VERTICAL PLANES INSIDE ESP

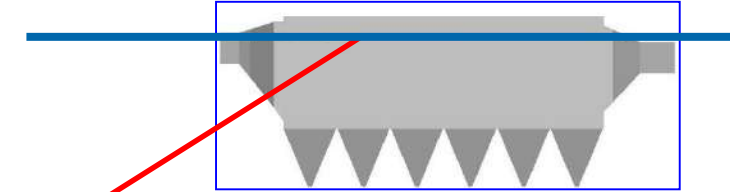
BASE

MOD

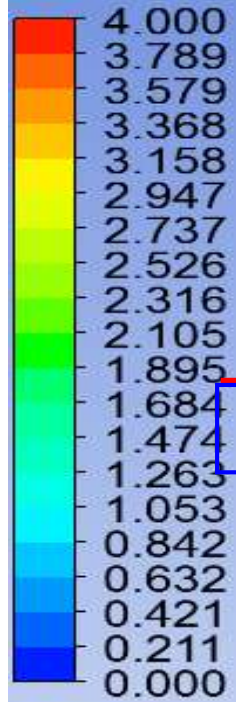


# EFFECT OF MODIFICATIONS ON FLOW PATTERN

HORIZONTAL PLANES CLOSE TO ESP TOP

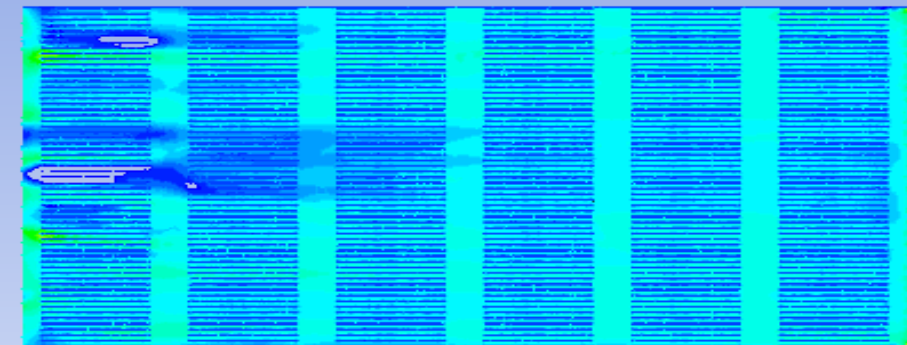
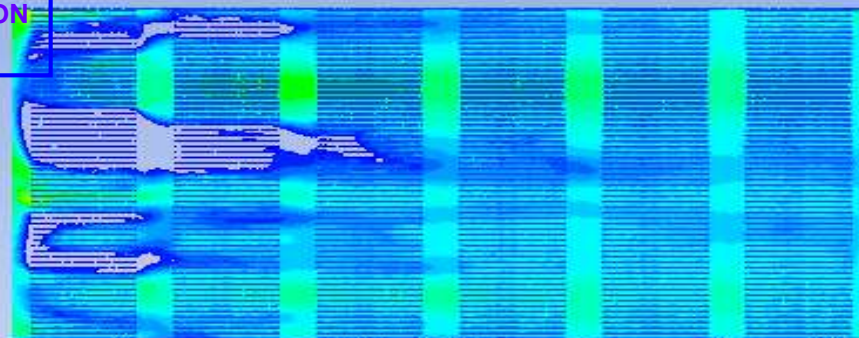
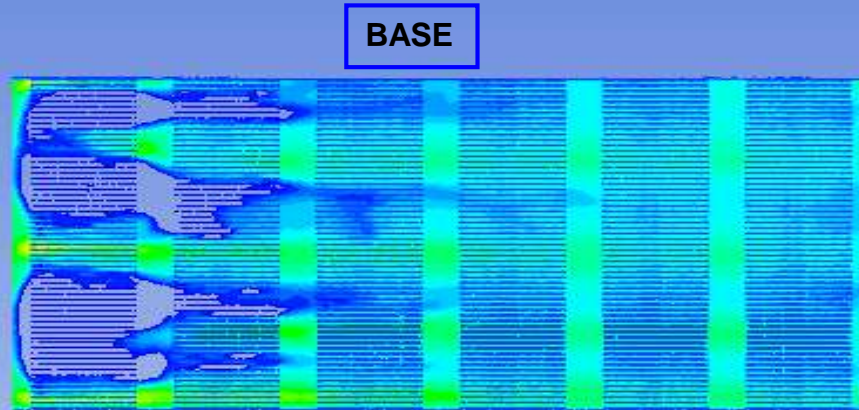


Velocity u  
Contour 1



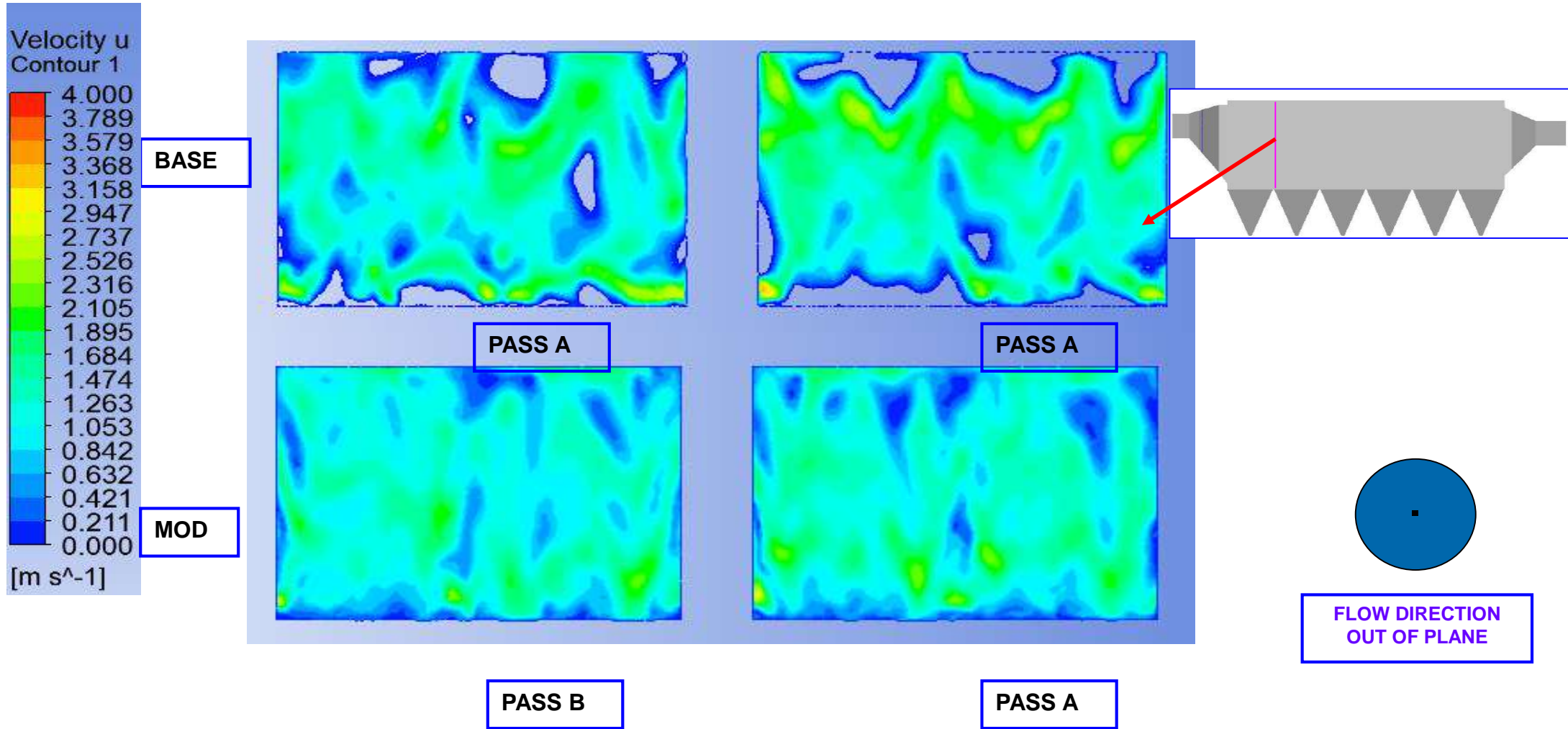
[m s<sup>-1</sup>]

FLOW DIRECTION  
X-AXIS



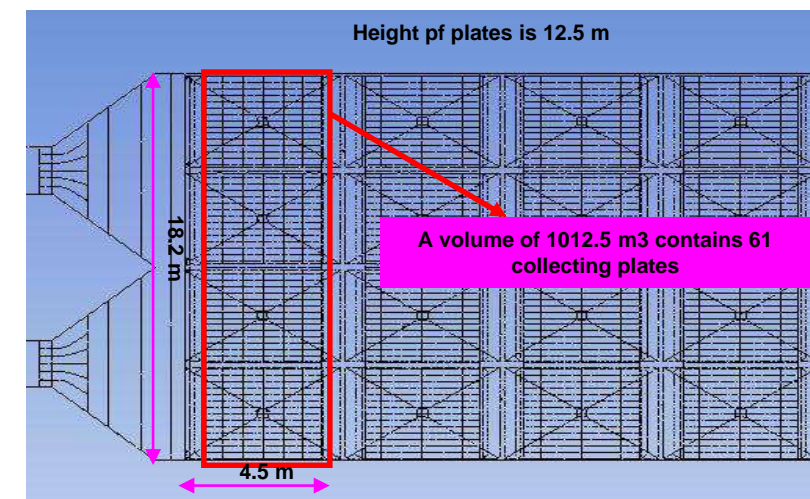
# EFFECT OF MODIFICATIONS ON FLOW PATTERN

## CROSS-SECTION AFTER FIRST FIELD



## Increase in Available Collecting Area of Plates

- **Recirculation/stagnation zones eliminated in modified case: 1000 m<sup>3</sup>**
- **Additional collection area being made available: 6750 m<sup>2</sup>**
- **Equivalent to adding one field in one pass**
  - 1000 m<sup>3</sup> of swept volume ~60 collecting plates
  - Additional Collecting area equivalent to 1000 m<sup>3</sup> ~ 6750 m<sup>2</sup>
  - (2 side of plate\*60 plates\*12.5 m height of each plate\*4.5 m width of each plate)



Equivalent to adding one field in any one pass



## EFFECT OF MODIFICATIONS ON FLOW PATTERN : SUMMARY

Decrease in Average velocity increasing residence time

| SN | Case     | % Area $\leq 1.15 V_{avg}$ | % Area $\leq 1.40 V_{avg}$ |
|----|----------|----------------------------|----------------------------|
| 1  | As built | 43.53                      | 62.27                      |
| 2  | Modified | 62.51                      | 86.59                      |

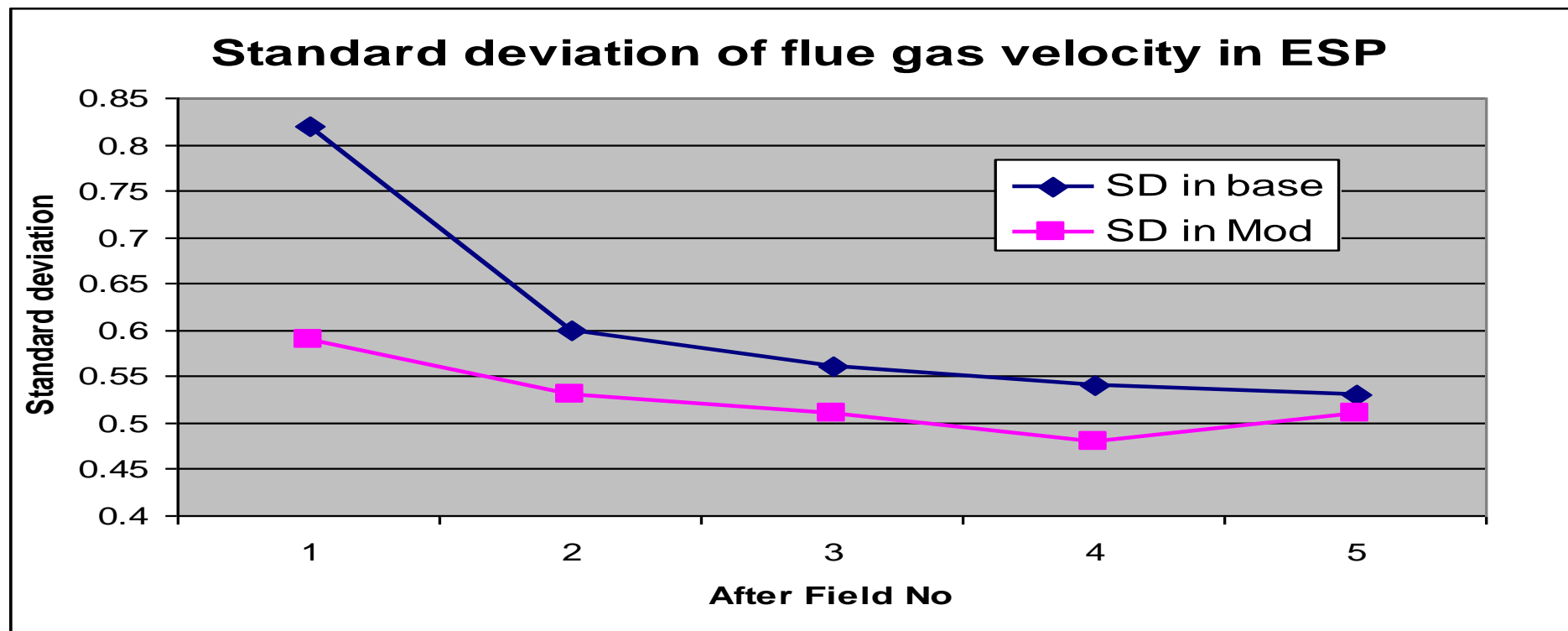
Velocity measurement plane: After First Field

The ICAC guidelines of publication EP-7 requires

"Within the treatment zone near the inlet and outlet faces of the precipitator collection chamber, the velocity pattern shall have

- 85 % of the velocities not more than 1.15 times the average velocity, and
- 99 % of the velocities not more than 1.40 times the average velocity"

## Standard Deviation of Velocity decreases in proposed modification



- In proposed modification standard deviation decreases, i.e., velocity uniformization
- Flow gets settled after second field both in Base and Modified case
- Weak effect of velocity subsequent first field on the overall efficiency of the ESP.

### Estimated improvement in SPM after modifications

- With respect to increased SCA, the calculated SPM after modification ~ 100 mg/Nm<sup>3</sup>
- With pressure drop reduction due to improved flow ~ 6 mm WC

### Modifications carried out:

- Carried out in major overhauling of U#4 in Jan 2018
- BHEL supplied the modified GD Screens
- Measurement was carried out by M/s SGS in June 2018
- Total cost of Modification including supply and services ~2.5 Cr

## ESP performance efficiency improvement by CFD modeling: CONCLUSIONS

- Flow abnormality exists at ESP inlets with unequal flow in passes (was not there in this case)
- Existing splitter plates not able to prevent separation and stagnation of flow
- Existing design GD screen do uniformize the flow but creates a stagnation zone in 1<sup>st</sup> and 2<sup>nd</sup> field
- The above flow abnormality decreases the effective SCA decreasing the capture efficiency
- CFD modeling is an ideal tool to predict and correct these flow abnormalities
- The cost of rectification based on CFD modeling is comparatively cheaper with respect to adding SCA by adding fields or passes
- CFD based modifications may be implemented before taking ESPs into R&M
- CFD modeling analysis may also be taken as design tool for finalizing SCA in new ESPs

**THANK YOU**



# CFD MODELING ASSUMPTIONS

- The flue gas flow has been considered to be single phase, steady and incompressible.
- No energy transfer has been considered across duct's and ESP's walls hence density and viscosity remains constant.
- Constituent species of the flue gas have not been considered.
- Mass flow distribution across the model inlet boundary is uniform.
- All the existing guide vanes and braces have been modeled as zero thickness wall.

# CFD MODELING MATHEMATICAL APPROACH

❖ Conservation of mass

$$\text{Mass : } \frac{\partial \rho}{\partial t} + \text{div}(\rho \mathbf{u}) = 0$$

❖ Conservation of momentum

## Turbulent flow - Reynolds equations

$$\begin{aligned} x - \text{momentum : } \quad & \frac{\partial(\rho U)}{\partial t} + \text{div}(\rho U \mathbf{U}) = -\frac{\partial P}{\partial x} + \text{div}(\mu \text{ grad } U) + S_{Mx} \\ & + \left[ -\frac{\partial(\overline{\rho u'^2})}{\partial x} - \frac{\partial(\overline{\rho u'v'})}{\partial y} - \frac{\partial(\overline{\rho u'w'})}{\partial z} \right] \end{aligned}$$

$$\begin{aligned} y - \text{momentum : } \quad & \frac{\partial(\rho V)}{\partial t} + \text{div}(\rho V \mathbf{U}) = -\frac{\partial P}{\partial y} + \text{div}(\mu \text{ grad } V) + S_{My} \\ & + \left[ -\frac{\partial(\overline{\rho u'v'})}{\partial x} - \frac{\partial(\overline{\rho v'^2})}{\partial y} - \frac{\partial(\overline{\rho v'w'})}{\partial z} \right] \end{aligned}$$

$$\begin{aligned} z - \text{momentum : } \quad & \frac{\partial(\rho W)}{\partial t} + \text{div}(\rho W \mathbf{U}) = -\frac{\partial P}{\partial z} + \text{div}(\mu \text{ grad } W) + S_{Mz} \\ & + \left[ -\frac{\partial(\overline{\rho u'w'})}{\partial x} - \frac{\partial(\overline{\rho v'w'})}{\partial y} - \frac{\partial(\overline{\rho w'^2})}{\partial z} \right] \end{aligned}$$

❖ Standard k - ε model has been used for the closure of turbulent momentum equations

# DETAIL OF RAMAGUNDAM ST-II ESP-Assumption

- All four ESP passes are geometrically similar and hence only one pass has been considered for modeling
- Zero thickness of collecting electrode plates.
- Six collecting plates in a row of a field have been merged in single plate as the gap is very small.
- Primary and secondary GD screen modeled as porous jump.
- Emitting electrode not modeled.
- Mass flow at the inlet is uniform.
- Support structure of the electrodes/rapping arrangements omitted from the model.



# DETAIL OF RAMAGUNDAM ST-II ESP-Ash Resistivity



Milling & Combustion Evaluation of Indian Steaming Coals: Ramagundam

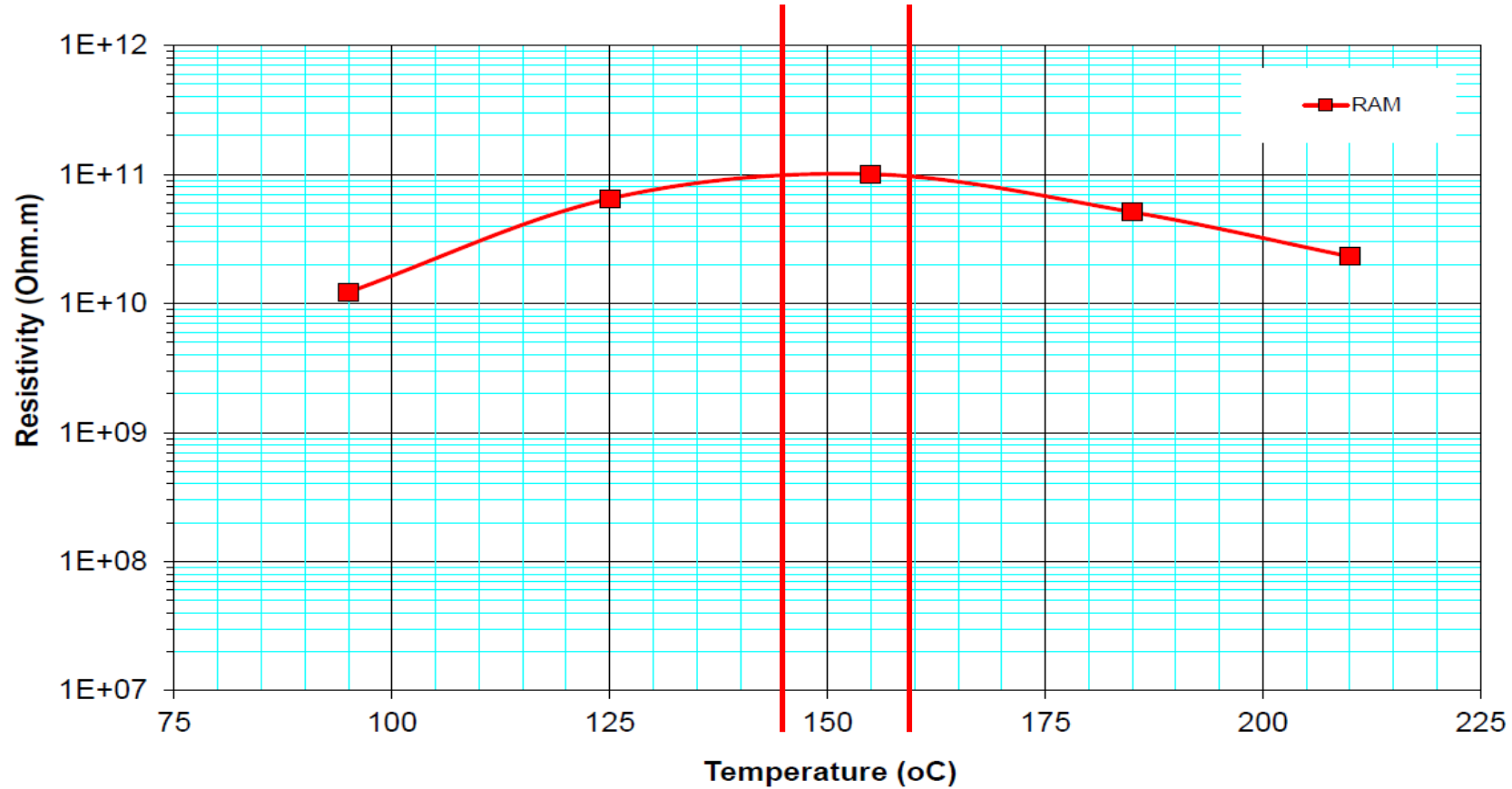


Fig. 6.3: Resistivity of RAM Fly Ash